

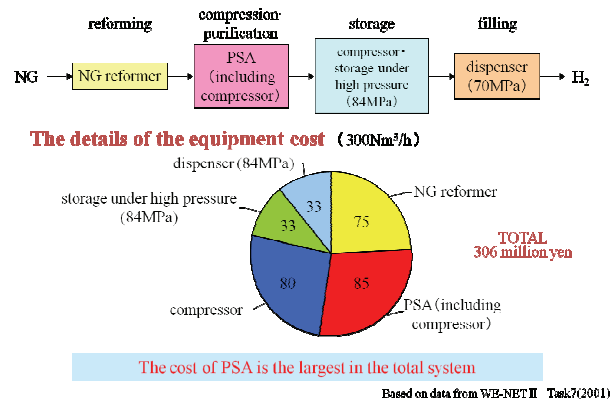


Fig.1 Schematic flow and equipment cost of H₂ station for Natural Gas reforming system

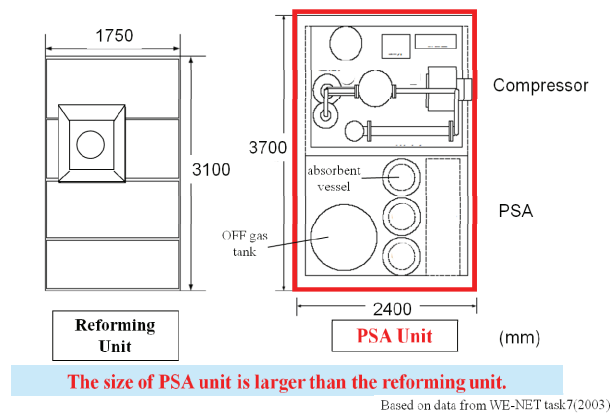


Fig.2 The area occupied by reforming and PSA units of H₂ station

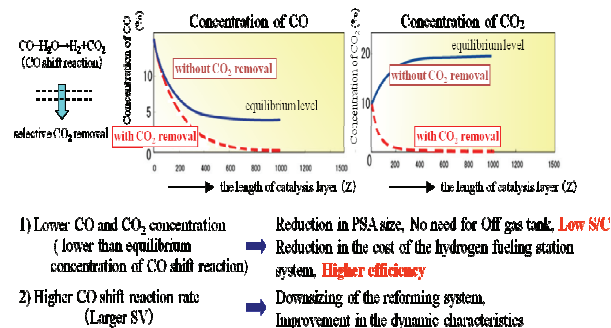


Fig.3 Effect of CO₂-selective membrane on CO shift reaction

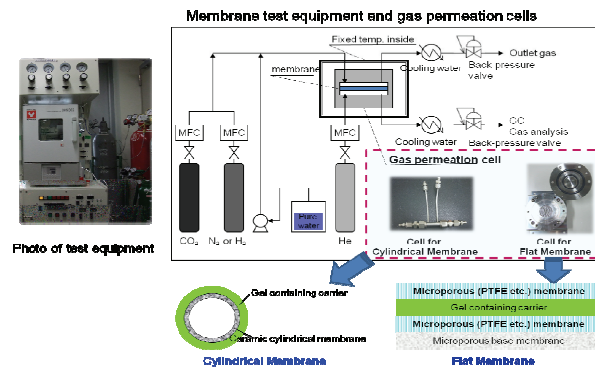


Fig.4 Evaluation method for CO₂ selective membrane

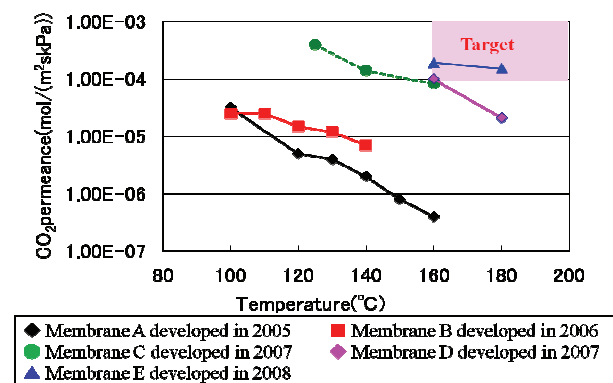


Fig.5 Performances of the developed CO₂-selective membranes (CO₂ permeance)

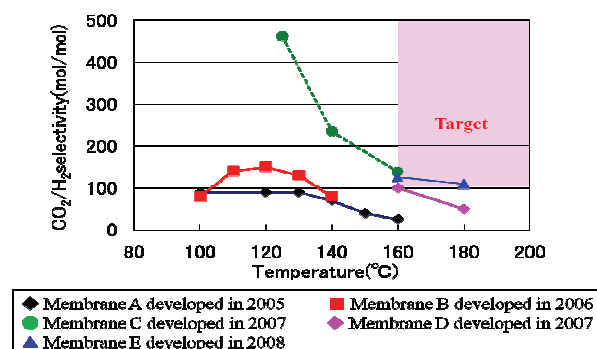


Fig.6 Performances of the developed CO₂-selective membranes(CO₂/H₂ selectivity)

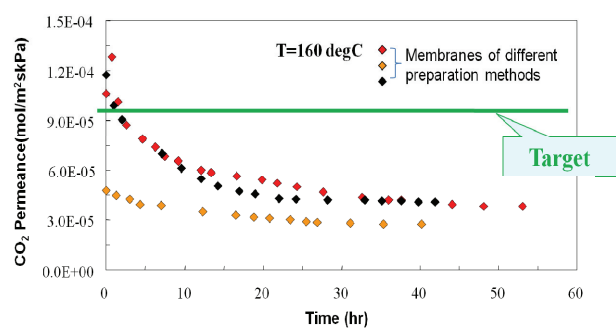


Fig.7 Results of durability test of CO₂ selective membranes

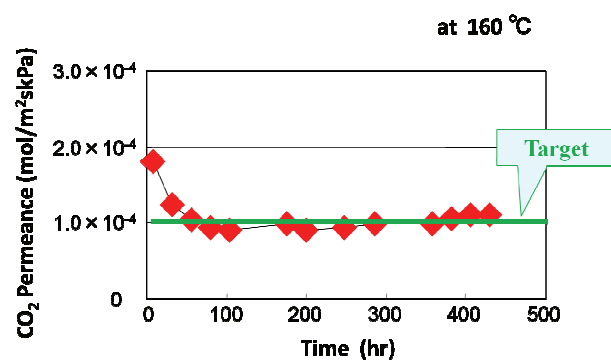


Fig.8 Result of durability test of improved membrane

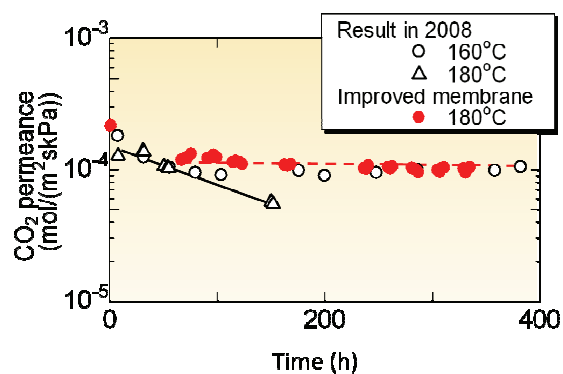


Fig.9 The stability of CO₂ membrane

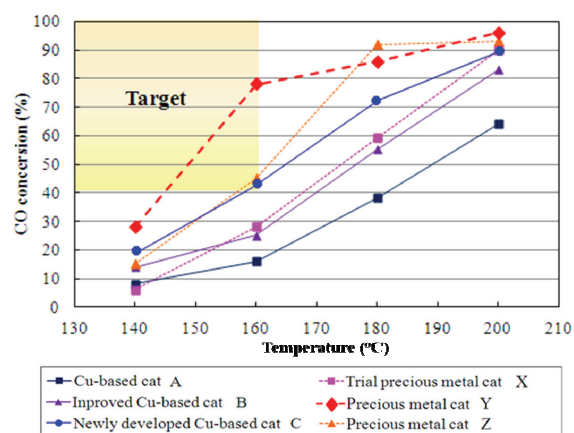


Fig.10 Development of highly active catalysts for CO shift in low temperature

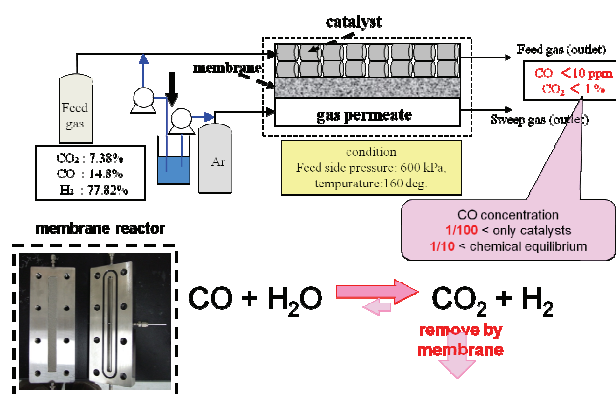


Fig.11 Performance of CO shift membrane reactor

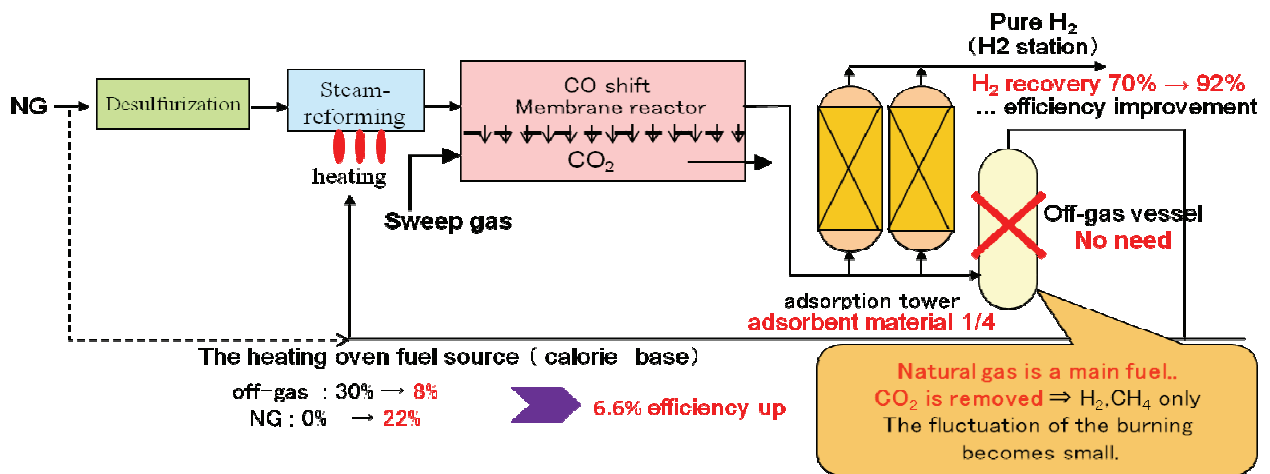


Fig.12 Effects for total system of membrane reactor

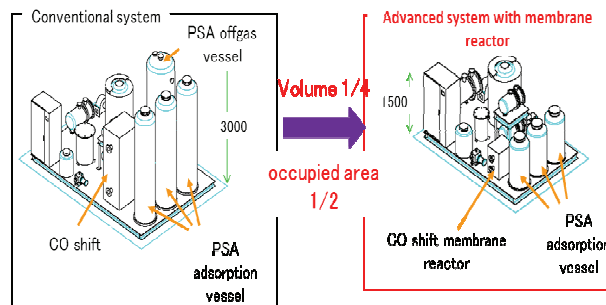


Fig.13 The arrangement of H₂ station (300Nm³/h)